

# Oxygen-free Conversion of Methane to Higher Hydrocarbons through a Dual-Temperature Two-Step Reaction Sequence on Platinum and Ruthenium

## 2. Removal of Products at a Fixed Temperature

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In order to study the effect of the temperature ( $T_{\text{CH}_4}$ ) at which the catalysts were exposed to  $\text{CH}_4$  upon the  $\text{C}_{2+}$  products of the further hydrogenation, the latter process was conducted at a fixed temperature ( $T_{\text{H}_2}$ ) while different values were ascribed to  $T_{\text{CH}_4}$  in a set of successive experiments.  $T_{\text{CH}_4}$  did not exceed  $320^\circ\text{C}$ . Different sets were effected, corresponding to different values of  $T_{\text{H}_2}$  (from room temperature to  $200^\circ\text{C}$ ). If  $T_{\text{H}_2} \leq 120^\circ\text{C}$  hydrogenolysis was negligible, so that the variations of the production were only due to the changes affecting the adlayer. On both catalysts and at every value of  $T_{\text{H}_2}$ , the production displayed a maximum versus  $T_{\text{CH}_4}$ . On Pt, the selectivity to ethane and propane at a given  $T_{\text{H}_2}$  monotonically decreased when  $T_{\text{CH}_4}$  increased while that corresponding to the heavier products ( $\text{C}_6\text{--}\text{C}_8$ ) increased. In contrast, on Ru, the selectivities to ethane and propane exhibited a minimum versus  $T_{\text{CH}_4}$  while those to heptanes and octanes exhibited a maximum. The results are interpreted by assuming that, during the chemisorption of  $\text{CH}_4$ , several families of hydrocarbon precursors of different weights and shapes are formed on the metal surfaces. It must be assumed that, on Pt, the average weight of the precursors was an increasing function of  $T_{\text{CH}_4}$ , whereas on Ru it displayed an optimum in the upper part of the explored range of  $T_{\text{CH}_4}$ . No appreciable amount of unreactive carbon was formed under the conditions of the described experiments. © 1998 Academic Press

## INTRODUCTION

In our preceding contribution (1) we have reported a part of the results obtained with silica-supported Pt and Ru catalysts by feeding them successively with  $\text{CH}_4$  and  $\text{H}_2$ . We have mainly been interested in dual-temperature experiments and especially in various series of experiments comprising a given exposure to  $\text{CH}_4$  at a fixed temperature,  $T_{\text{CH}_4}$ , as a first step, followed by hydrogenation/desorption of the resulting adspecies at a lower temperature,  $T_{\text{H}_2}$ , as a second step. The interest of this approach lies in the fact

that only the second step was responsible for the variations of the amount of the homologated  $\text{CH}_4$  and of the product distribution since the adlayer resulting from the first step remained the same in a given series of experiments.

We are now reporting on the results of complementary experiments whose second steps (hydrogenations) have been carried out at a fixed  $T_{\text{H}_2}$  in a given series, following exposures to  $\text{CH}_4$  conducted at various  $T_{\text{CH}_4}$  in the successive experiments of the series. So doing, the changes affecting the results could originate but in the modifications undergone by the adlayer, due to the choice of  $T_{\text{CH}_4}$ . Moreover, by adequately choosing  $T_{\text{H}_2}$ , the hydrogenolysis of the products could be rendered negligible.

The composition of the adlayer resulting from exposure of a metal surface to molecules able to give rise to chemisorbed carbonaceous species is expected to depend upon the nature of the metal, that of the molecules, and the conditions of the exposure. In catalytic studies it has become a common practice to submit the adspecies to TPSRs (temperature programmed surface reactions) in order to get a kind of fingerprint of the possible various species present on the surface. In the case of surfaces exposed to hydrocarbons, different forms of C are expected from decomposition of the species. It is frequently in terms such as  $\text{C}_\alpha$ ,  $\text{C}_\beta$ , and  $\text{C}_\gamma$  that the composition of the adlayer is described, due to the frequent presence of three main methane peaks in the  $\text{H}_2$ -TPSR. To our knowledge, McCarty and Wise were the first to adopt this terminology in a study devoted to the case of an alumina-supported Ni catalyst (2). However, only two peaks resulted from an exposure to CO. The first one, which they called  $\text{C}_\alpha$ , exhibited its maximum at  $T_p \approx 200^\circ\text{C}$  and the second one, named  $\text{C}_\beta$ , occurred at  $T_p \approx 400^\circ\text{C}$ , but it was very broad and extended itself above  $600^\circ\text{C}$ . A third peak, named  $\text{C}_\gamma$  (at  $T_p \approx 280^\circ\text{C}$  and partly overlapping  $\text{C}_\alpha$ ) was formed upon exposure of the same catalyst to  $\text{C}_2\text{H}_4$ . Another peak,  $\text{C}_{\alpha'}$ , could appear as a shoulder on the ascending branch of  $\text{C}_\alpha$  and originated in a very reactive form

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of carbon deposit able to react from  $\approx 50^\circ\text{C}$  or even room temperature (r.t.). They proposed to identify  $C_\alpha$  as isolated carbon atoms, possibly  $C_2$ , bonded to Ni atoms,  $C_{\alpha'}$  as a similar species, but bonded to surface defects,  $C_\beta$  as a polymerized form of carbon like that already described as consisting of graphitic domains, about 15 Å in size, on Ni(110) (3–5) and Ni(001) (6).  $C_\gamma$ , formed only from ethylene in their study, was identified as superficial  $\text{Ni}_3\text{C}$ .

The carbonaceous species present on the surface of silica-supported Ru catalysts under the conditions of Fischer–Tropsch synthesis have been extensively studied by Bell's group. Four forms of nonoxygenated adspecies were identified with isotopic tracers and  $^{13}\text{C}$  NMR spectroscopy (7–11). One form,  $C_\alpha$ , also called carbidic carbon, was considered to be easily convertible to  $\text{CH}_4$  and higher alkanes. Another form,  $C_\beta$ , was viewed as constituted of two kinds of alkyl groups,  $C_{\beta 1}$  and  $C_{\beta 2}$ , differing by their mobilities on the surface and, finally, the unreactive graphitic carbon was called  $C_\gamma$ . In a further study devoted to the case of a  $\text{TiO}_2$ -supported Ru catalyst, the  $C_\beta$  species was differentiated into  $C_{\beta'}$ , intermediate to  $C_{2+}$  alkanes, and  $C_{\beta''}$ , supposed to consist of longer alkyl chains residing on the support (12).

In their contribution to the study of the possible conversion of  $\text{CH}_4$  to higher alkanes by a two-step reaction sequence, Koerts *et al.* also recognized three classes of carbonaceous adspecies to which similar names were ascribed (13). These authors considered that  $C_\alpha$  is the adspecies whose hydrogenation leads to the formation of  $C_{2+}$  alkanes and, in agreement with the previous NMR studies by Bell *et al.*, they also considered that  $C_\alpha$  has only metal atoms in its first coordination shell.

In the case of a silica-supported Ru catalyst, exposed to a single or successive pulses of  $\text{CH}_4$ , Carstens and Bell observed the possible formation of  $C_\alpha$ , hydrogenatable at less than  $100^\circ\text{C}$ ,  $C_\beta$ , hydrogenatable between about 120 and  $350^\circ\text{C}$  and  $C_\gamma$ , the least reactive form of carbon ( $T_p > 400^\circ\text{C}$ ), interpreted as graphitic carbon (14). The proportions of these different adspecies were obviously dependent upon the conditions of their formation. A more detailed examination allowed the authors to subcategorize  $C_\alpha$  into  $C_{\alpha 1}$ , which could react at r.t. (or less) and  $C_{\alpha 2}$ , reacting between r.t. and  $100^\circ\text{C}$ .  $C_\beta$  could also be subcategorized into three adspecies, i.e.  $C_{\beta 1}$  and  $C_{\beta 3}$ , only formed on carburized Ru, and  $C_{\beta 2}$ , formed on carburized or noncarburized Ru. Due to aging in stagnant He,  $C_{\beta 1}$  could give rise to  $C_\gamma$ . Aging also caused the growth of  $C_{\alpha 2}$  and  $C_{\beta 1}$  at the expense of  $C_{\beta 2}$  while  $C_\gamma$  seemed to be irreversibly formed. Ethane was the main homologated product and was mostly released from carburized ruthenium on which  $C_\alpha$  and  $C_\gamma$  were more favored than  $C_\beta$ .

A great deal of surface science studies, using the electron spectroscopies commonly associated with them, has been accomplished to identify the various carbonaceous adspecies able to be formed on metal surfaces mainly, but not

uniquely, from exposures to  $(\text{CO} + \text{H}_2)$ . The corresponding contributions published before 1981 were reviewed by Biloen and Sachtler (15). At least two of their results are directly related to the subject of the present work. One is that two main kinds of deposits can be distinguished: a little reactive graphitic carbon and a much more reactive adspecies named carbidic carbon. The second is that the carbidic carbon is heterogeneous in nature since it can consist of adsorbed carbon atoms,  $\text{CH}_x$  adspecies, and polymeric units involving C–C bonds. Graphitic carbon can therefore be unambiguously classed as  $C_\gamma$ , whereas carbidic carbon may encompass  $C_\alpha$  as well as  $C_\beta$  if  $C_\alpha$  is considered to be deprived of C–C bondings. Among the more recent reports we attach a particular significance to those revealing differences between the results of exposures to either CO (possibly added to  $\text{H}_2$ ) or hydrocarbonaceous molecules (16, 17) and also to those which show the existence of C–C bondings between adspecies stemming from exposures to methane prior to the supply of hydrogen. The latter case is illustrated in the contribution by Wu and Goodman (18) concerning the adsorption of  $\text{CH}_4$  on Ru(0001) and Ru(11 $\bar{2}$ 0). From detailed examination of various spectroscopic results concerning carbidic layers formed on Ni(100) and Ni(111) during exposures to CO or to  $\text{C}_2\text{H}_4$ , Hutson *et al.* concluded that significant amounts of C–C bonds were present on the surface, thus revealing the existence of adspecies containing 2, 3, or more carbon atoms (19).

We will now report on our results and we will try to show how they can give some insight into the composition of the adlayers originating in  $\text{CH}_4$  chemisorption on Pt and Ru.

## PROCEDURES AND CATALYSTS

The apparatus, the methods and the catalysts samples are exactly those which have been described in the preceding article (1).

## RESULTS

Increasing coverages of the metal surface were expected from exposures to  $\text{CH}_4$  conducted at increasing temperatures in successive separate experiments, other experimental conditions being fixed. We will essentially consider here the results of hydrogenations at fixed  $T_{\text{H}_2}$  (total  $C_{2+}$  productions and product distributions successively) and report their variations with  $T_{\text{CH}_4}$ . We will pursue by reporting the results of  $\text{H}_2$ -TPSR's following exposures to  $\text{CH}_4$  conducted at various temperatures.

### 1. Experiments Corresponding to a Fixed $T_{\text{H}_2}$

#### 1.1. $C_{2+}$ Productions

Figures 1 and 2, respectively, represent the results obtained at  $T_{\text{H}_2} = 100^\circ\text{C}$  on Pt and  $T_{\text{H}_2} = 120^\circ\text{C}$  on Ru. They give

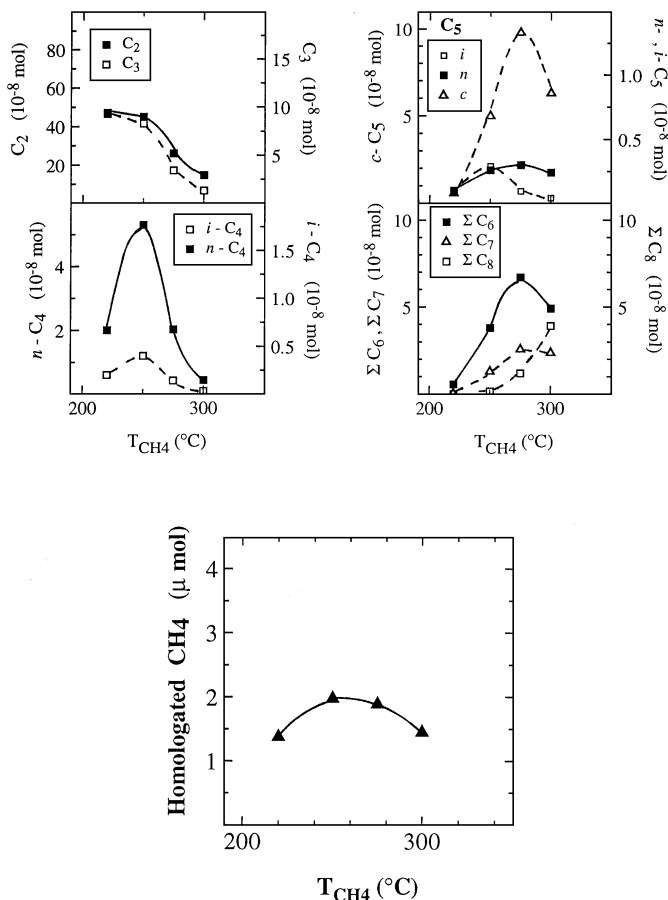


FIG. 1. Variations with  $T_{CH_4}$  of the molar amounts of the total homologated methane and of the various  $C_{2+}$  alkanes resulting from the exposure of 100 mg of **EUROPT-1** to methane at  $T_{CH_4}$  (step 1) and subsequent hydrogenation at a fixed  $T_{H_2}$  (100°C) (step 2). Conditions: Step 1, exposure to  $CH_4$  (1 bar, 400  $cm^3$   $min^{-1}$ , 1 min,  $T_{CH_4}$ ); Step 2, exposure to  $H_2$  (1 bar, 50  $cm^3$   $min^{-1}$ , 100°C).

the detailed productions of the various  $C_{2+}$  hydrocarbons, as well as the total amounts of homologated  $CH_4$ . Except for one particular value of  $T_{CH_4}$  for each metal (300 and 240°C for Pt and Ru, respectively) the detailed productions reported here have not been given in our previous contribution (1). The total amounts of homologated  $CH_4$  can be found among the data of our previous contribution but it is natural and useful to plot them here versus  $T_{CH_4}$  whose effect is specifically studied in the present work. For both metals, most remarkably, the total  $C_{2+}$  production exhibited a maximum versus  $T_{CH_4}$  which was more pronounced, however, in the case of Ru. On this latter metal, corresponding maxima were also present in the productions of each  $C_{2+}$  product, but on Pt such was not the case for ethane and propane which monotonically decreased and for the octanes which increased through the whole range of temperatures. The  $T_{CH_4}$  values maximizing each alkane production tended to increase with the weight of the alkane.

Results quite similar to the preceding ones were obtained with each metal at other settings of  $T_{H_2}$ . The corresponding total  $C_{2+}$  productions versus  $T_{CH_4}$  are collected in Figs. 3 and 4. As concerns Pt (Fig. 3), the curves showed a maximum at approximately the same value of  $T_{CH_4}$  (260–265°C), irrespective of the value of  $T_{H_2}$ . Octanes were formed even at r.t. if  $T_{CH_4}$  was higher than 275°C, whereas a maximum appeared for ethane and propane if  $T_{H_2}$  was fixed at 200°C. On Ru (Fig. 4), at  $T_{H_2}$  equal to 22 or 80°C, only the decreasing branch of the curve representing the variations of the amount of the total homologated methane versus  $T_{CH_4}$  was obtained, which reflected the same situation than for the detailed curves corresponding to each  $C_2$  to  $C_5$  alkane. The curves displayed neat maxima if  $T_{H_2}$  equalled 120 or 160°C. As well in Fig. 3 as in Fig. 4 the points represented as big circles correspond to isothermal experiments and are given for the sake of comparison.

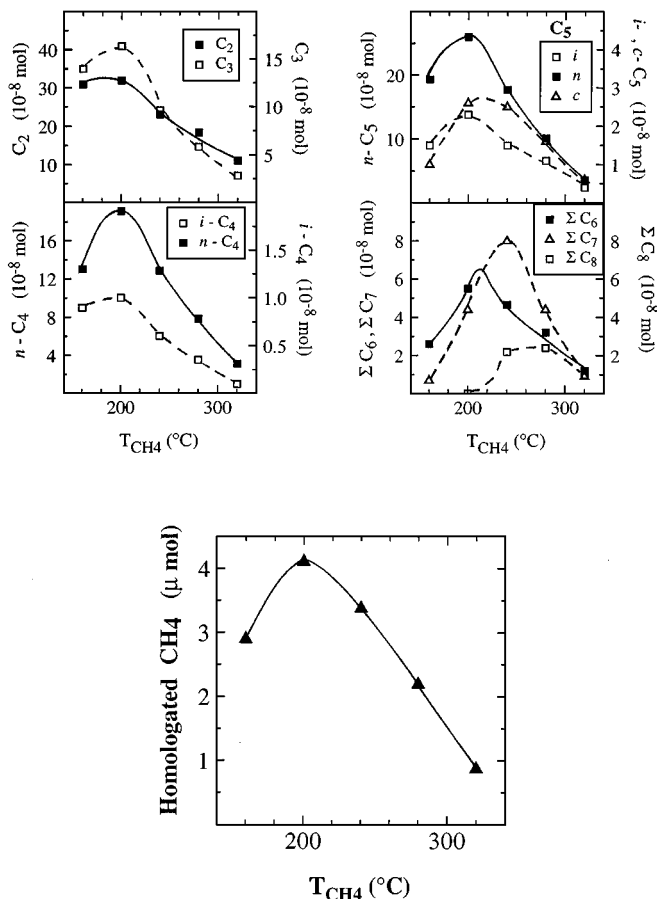
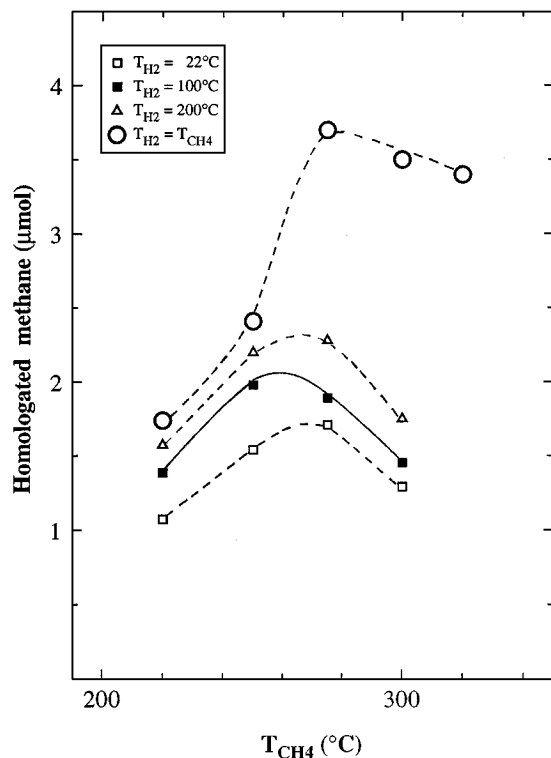


FIG. 2. Variations with  $T_{CH_4}$  of the molar amounts of the total homologated methane and of the various  $C_{2+}$  alkanes resulting from the exposure of 100 mg of **Ru/SiO<sub>2</sub>** to methane at  $T_{CH_4}$  (step 1) and subsequent hydrogenation at a fixed  $T_{H_2}$  (120°C) (step 2). Conditions: Step 1, exposure to  $CH_4$  (1 bar, 375  $cm^3$   $min^{-1}$ , 5 min,  $T_{CH_4}$ ); Step 2, exposure to  $H_2$  (1 bar, 50  $cm^3$   $min^{-1}$ , 120°C).



**FIG. 3.** Variation with  $T_{\text{CH}_4}$  of the molar amount of the total homologated methane resulting from an exposure of 100 mg of **EUROPT-1** to methane at  $T_{\text{CH}_4}$  (step 1) and subsequent hydrogenation at a fixed  $T_{\text{H}_2}$  (step 2). The different curves correspond to different values of  $T_{\text{H}_2}$ . Conditions: Step 1, exposure to  $\text{CH}_4$  (1 bar,  $400 \text{ cm}^3 \text{ min}^{-1}$ , 1 min,  $T_{\text{CH}_4}$ ); Step 2, exposure to  $\text{H}_2$  (1 bar,  $50 \text{ cm}^3 \text{ min}^{-1}$ ,  $T_{\text{H}_2}$  fixed).

### 1.2. Product Distributions

On Pt, there was a continuous and dramatic decrease of the selectivities to ethane and propane if  $T_{\text{CH}_4}$  was given increasing values at a fixed  $T_{\text{H}_2}$ . For example, one can see in Fig. 5, which is the bar chart corresponding to Fig. 1 ( $T_{\text{H}_2} = 100^\circ\text{C}$ ), that the selectivity to ethane decreased from  $\approx 68$  to  $\approx 20\%$  (while the corresponding values for propane were  $\approx 20$  and  $2.6\%$ ) if  $T_{\text{CH}_4}$  was increased from 220 to  $300^\circ\text{C}$ . The selectivities to butanes, pentanes, and hexanes exhibited maxima. For instance,  $\approx 21\%$  of the homologated  $\text{CH}_4$  was involved in hexanes at  $T_{\text{CH}_4} = 275^\circ\text{C}$ . The selectivities to heptanes and octanes increased regularly up to  $21.6\%$  at  $T_{\text{CH}_4} = 300^\circ\text{C}$ .

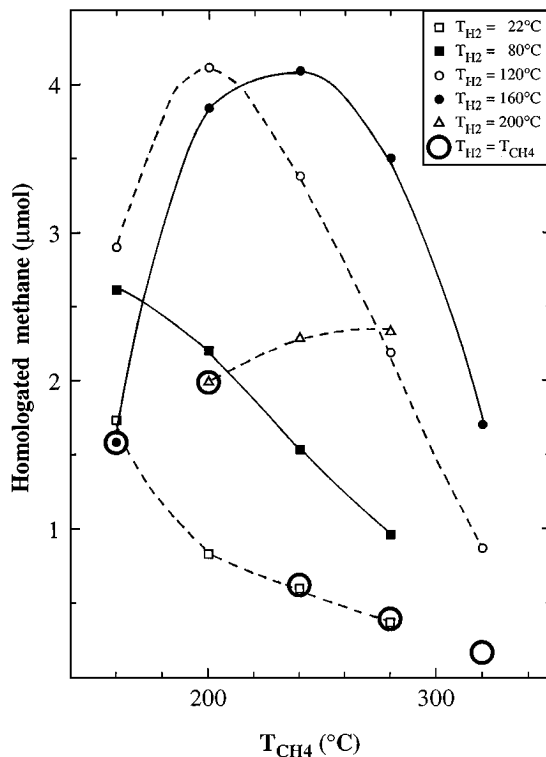
On Ru, when  $T_{\text{CH}_4}$  was given increasing values at a fixed  $T_{\text{H}_2}$ , the selectivities to ethane and propane first decreased, displayed a minimum, and then re-increased. For instance, in the case represented in Fig. 6, which is the bar chart corresponding to Fig. 2 ( $T_{\text{H}_2} = 120^\circ\text{C}$ ), the selectivity to ethane decreased from  $\approx 21\%$  ( $T_{\text{CH}_4} = 160^\circ\text{C}$ ) to  $13.5\%$  ( $T_{\text{CH}_4} = 240^\circ\text{C}$ ) and re-increased to  $\approx 25\%$  ( $T_{\text{CH}_4} = 320^\circ\text{C}$ ). The selectivity to the butanes decreased slowly throughout the range of variation of  $T_{\text{CH}_4}$ , whereas that to the pentanes decreased monotonically from  $\approx 38\%$  ( $T_{\text{CH}_4} = 160^\circ\text{C}$ )

to  $\approx 26\%$  ( $T_{\text{CH}_4} = 320^\circ\text{C}$ ). The selectivity to the hexanes underwent little changes while the selectivity to the heptanes exhibited a maximum ( $\approx 17\%$  to heptanes at  $T_{\text{CH}_4} = 240^\circ\text{C}$ ). The octanes did not appear at 160 and  $200^\circ\text{C}$  and represented ca  $10\%$  at 280 and  $320^\circ\text{C}$ .

A remarkable point of these results (as of all our previous results) is that they exhibit strong departures from Anderson–Schultz–Flory (ASF) distribution. For example, after an initial exposure of Pt to  $\text{CH}_4$  at  $275^\circ\text{C}$ , more  $\text{CH}_4$  was involved in the formations of hexanes, heptanes, and octanes than in that of propane and butanes. On Ru, the same was true for the pentanes, as compared to ethane, propane, and butanes at any of the temperatures of Fig. 6. The same trends and strong departures from ASF distribution could be observed at any  $T_{\text{H}_2}$ , including r.t., as is shown by the bar charts represented in Figs. 7 and 8, corresponding to hydrogenations carried out at r.t. on Pt and Ru, respectively.

## 2. Results of Typical $\text{H}_2$ -TPSRs Following Exposures to $\text{CH}_4$

In order to check whether  $\text{C}_\gamma$  was present or not after the exposures of our catalysts to  $\text{CH}_4$  in the conditions



**FIG. 4.** Variation with  $T_{\text{CH}_4}$  of the molar amount of the total homologated methane resulting from an exposure of 100 mg of **Ru/SiO<sub>2</sub>** to methane at  $T_{\text{CH}_4}$  (step 1) and subsequent hydrogenation at a fixed  $T_{\text{H}_2}$  (step 2). The different curves correspond to different values of  $T_{\text{H}_2}$ . Conditions: Step 1, exposure to  $\text{CH}_4$  (1 bar,  $400 \text{ cm}^3 \cdot \text{min}^{-1}$ , 5 min,  $T_{\text{CH}_4}$ ); Step 2, exposure to  $\text{H}_2$  (1 bar,  $50 \text{ cm}^3 \cdot \text{min}^{-1}$ ,  $T_{\text{H}_2}$  fixed).

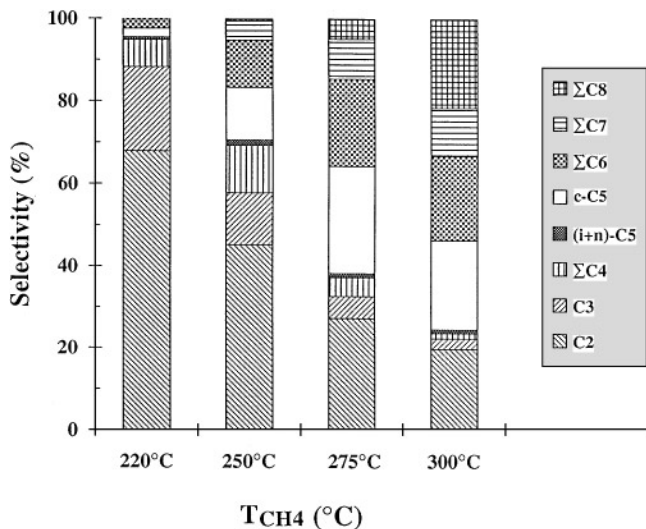


FIG. 5. Pt—Distribution of the homologated CH<sub>4</sub> in the C<sub>2+</sub> products for various T<sub>CH<sub>4</sub></sub>, T<sub>H<sub>2</sub></sub> being fixed at 100°C. Data are deduced from Fig. 1.

chosen for our experiments, we have carried out H<sub>2</sub>-TPSR's in the same way as that commonly used by other authors, that is to say without preliminary TPD's as we previously did (21, 22). Examples of such spectra are given in Figs. 9 and 10. Application of the heating program was preceded by a period of isothermal hydrogenation at r.t. (Figs. 9a, 9b and Figs. 10a) or at 100°C (Fig. 10b). The total C<sub>2+</sub> productions resulting from these isothermal parts of the hydrogenations at r.t. are given in Figs. 3 and 4. Figures 9 and 10 only illustrate the profiles of CH<sub>4</sub> and also of C<sub>2</sub>H<sub>6</sub> and C<sub>3</sub>H<sub>8</sub> which could accompany the release of methane and could be chromatographically monitored on line during the heating program. For the sake of brevity, we

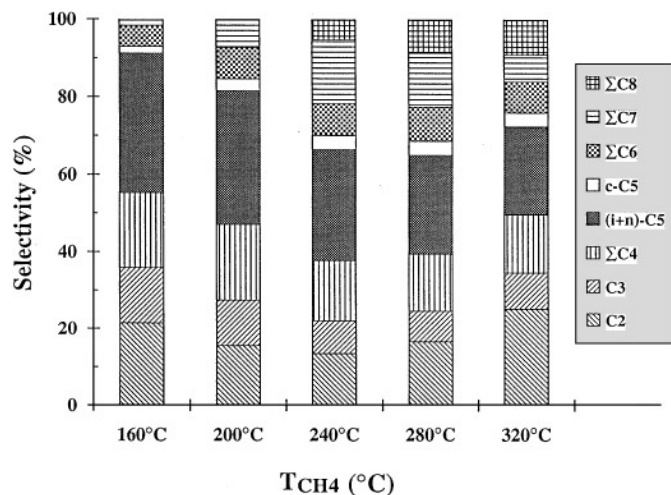


FIG. 6. Ru—Distribution of the homologated CH<sub>4</sub> in the C<sub>2+</sub> products at various T<sub>CH<sub>4</sub></sub>, T<sub>H<sub>2</sub></sub> being fixed at 120°C. Data are deduced from Fig. 2.

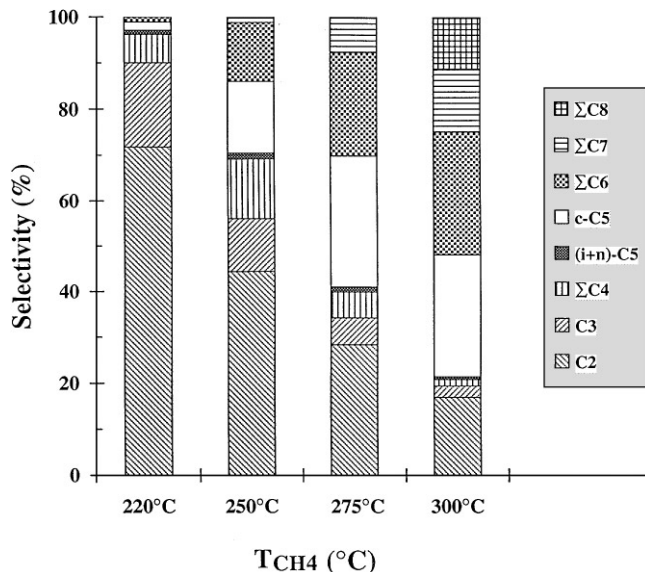


FIG. 7. Pt—Distribution of the homologated CH<sub>4</sub> in the C<sub>2+</sub> products for various T<sub>CH<sub>4</sub></sub>, T<sub>H<sub>2</sub></sub> being fixed at r.t. (other conditions being the same as for Fig. 5).

only report the profiles corresponding to two experiments concerning each catalyst. In the case of Pt, we have chosen two exposures carried out under the conditions here explored. Figure 9 shows how much the details of the profiles are sensitive to the temperature of the exposure. As concerns Ru, we have compared a profile generated by one of the present conditions with one corresponding to an elevated T<sub>CH<sub>4</sub></sub> (460°C) and a low pressure of CH<sub>4</sub> (0.007 bar).

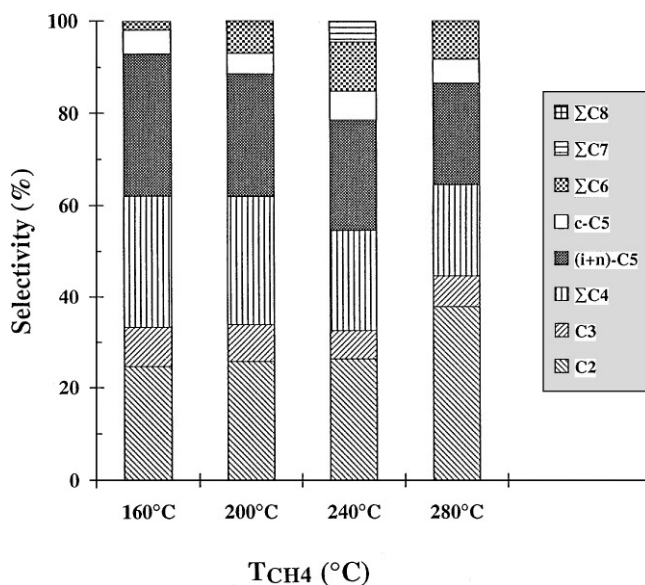


FIG. 8. Ru—Distribution of the homologated CH<sub>4</sub> in the C<sub>2+</sub> products at various T<sub>CH<sub>4</sub></sub>, T<sub>H<sub>2</sub></sub> being fixed at r.t. (other conditions being the same as for Fig. 6).

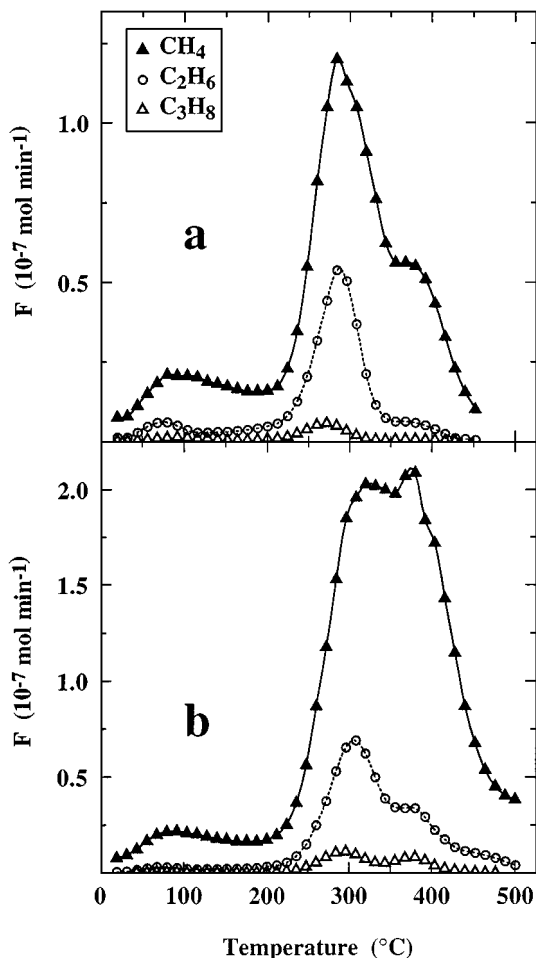


FIG. 9.  $\text{H}_2$ -TPSR of the carbonaceous species remaining on 100 mg of **EUROPT-1** after pre-adsorption of  $\text{CH}_4$  at 250°C (a), or 300°C (b), followed by hydrogenation at r.t. Conditions: Adsorption of  $\text{CH}_4$ : 1 bar,  $400 \text{ cm}^3 \text{ min}^{-1}$ , 1 min, 250°C (a), or 300°C (b). Isothermal hydrogenation: 1 bar,  $50 \text{ cm}^3 \text{ min}^{-1}$ , 15 min, r.t.  $\text{H}_2$ -TPSR: 1 bar,  $50 \text{ cm}^3 \text{ min}^{-1}$ ,  $8 \text{ K min}^{-1}$ .

Figure 10 clearly puts into evidence how the high-temperature part of the spectrum dramatically differs when the exposure to  $\text{CH}_4$  has been conducted under conditions allowing a large extent of  $\text{CH}_4$  decomposition.

#### DISCUSSION

As  $T_{\text{H}_2}$  was most often sufficiently low for allowing us to neglect the hydrogenolysis processes, only the differences concerning the content of the adlayer built up during the exposure to  $\text{CH}_4$  were responsible for those affecting the subsequent hydrocarbon release.

Only on Ru, did the  $\text{C}_{2+}$  production display a maximum versus  $T_{\text{H}_2}$  at a fixed  $T_{\text{CH}_4}$  (1). In the reverse present case, both metals display a maximum concerning as well the total  $\text{C}_{2+}$  production as the production of each product versus  $T_{\text{CH}_4}$  at a fixed  $T_{\text{H}_2}$ .

In Figs. 1 and 2 the rising parts of the curves are obviously due to the growth of the adlayer formed when  $T_{\text{CH}_4}$  is increased. The following decrease is much more surprising. At first sight we might consider that, if  $T_{\text{CH}_4}$  is increased, increasing amounts of unreactive carbon are formed on the catalysts, partly at the expense of reactive adspecies. However, the  $\text{H}_2$ -TPSR spectra (Figs. 9a, 9b, 10a) show that no  $\text{C}_\gamma$  was formed in our experiments. Moreover, if formation of  $\text{C}_\gamma$  was the reason of the decrease of the production of the higher alkanes, we would not have observed an increase of the latter total production upon hydrogenation at 100°C on Pt or 80°C on Ru, as compared to that at r.t., as shown in Figs. 3 and 4 since  $\text{C}_\gamma$  is not reacted at so low temperatures.

Due to the increase of  $T_{\text{CH}_4}$ , increasing concentrations of carbonaceous deposits are present on the surface at the

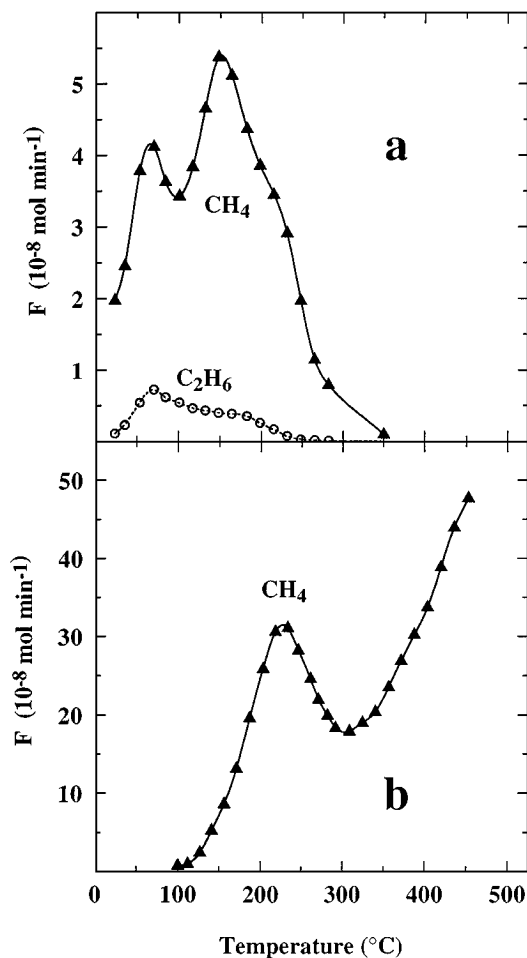


FIG. 10.  $\text{H}_2$ -TPSR of the carbonaceous species remaining on 100 mg of **Ru/SiO<sub>2</sub>** after pre-adsorption of  $\text{CH}_4$  at 260°C (a), or 460°C (b), followed by an isothermal hydrogenation at r.t. (a), or at 100°C (b). Conditions: Adsorption of  $\text{CH}_4$ : (a)  $\text{CH}_4$ , 1 bar,  $400 \text{ cm}^3 \text{ min}^{-1}$ , 5 min, 260°C; (b) (99.3% He, 0.7%  $\text{CH}_4$ ), 1 bar,  $50 \text{ cm}^3 \text{ min}^{-1}$ , 20 min, 460°C. Isothermal hydrogenation: (a) 1 bar,  $50 \text{ cm}^3 \text{ min}^{-1}$ , 10 min, r.t. (b) 1 bar,  $50 \text{ cm}^3 \text{ min}^{-1}$ , 15 min, 100°C.  $\text{H}_2$ -TPSR: 1 bar,  $50 \text{ cm}^3 \text{ min}^{-1}$ ,  $8 \text{ K min}^{-1}$  (a) or  $10 \text{ K min}^{-1}$  (b).

end of the exposure to  $\text{CH}_4$ . Higher concentrations are expected to favor association through C–C bonding but the reverse may also result from increased temperatures. Contrasting situations may then prevail, depending on whether the first or the second trend is predominant. Nevertheless both of them can give rise to a maximum of the  $\text{C}_{2+}$  production versus  $T_{\text{CH}_4}$ . That the second possibility can do so is obvious. Even if less obvious, the first one can also do the same. As seen in our preceding article (1), not all the heavy precursors are removed at a low or moderate  $T_{\text{H}_2}$  during the limited duration of the hydrogenation step. Increasing proportion of heavy precursors in the adlayer makes the latter less easily retrievable during the second step of the process and can thus also explain the progressive decrease of the  $\text{C}_{2+}$  amount.

We think that a growing association versus  $T_{\text{CH}_4}$  is predominant in the case of Pt. The tendency of the platinum surface to allow the formation of heavy precursors at increased temperatures of exposure to methane has already been evidenced in our preceding contribution (1). In agreement with that, the bar chart represented in the Fig. 5 of the present contribution evidences a strong decrease of the fraction of the converted methane involved in the ethane upon increasing  $T_{\text{CH}_4}$ ,  $T_{\text{H}_2}$  being fixed at  $100^\circ\text{C}$ . As  $\text{C}_2\text{H}_6$  is easily removed from the surface this decrease can only result from that of its  $\text{C}_2$  precursor among its accompanying adspecies. The same takes place for the propane and the butanes but just the opposite is observed for the  $\text{C}_{5+}$  products which eventually represent more than 75% of the homologated methane. The most dramatic variations are those exhibited by the heptanes and, above all, the octanes which are nonexistent if the exposure to  $\text{CH}_4$  is carried out at  $220^\circ\text{C}$ , but which represent about 25% of the homologated methane if  $T_{\text{CH}_4} = 300^\circ\text{C}$ .

On the contrary, the Ru catalyst appears to illustrate that less C–C bonding tends to occur at increased  $T_{\text{CH}_4}$ . Let us first point out in the bar chart of Fig. 6 the remarkable variation of the selectivity to ethane which exhibits a minimum at  $T_{\text{CH}_4} = 240^\circ\text{C}$ ,  $T_{\text{H}_2}$  being fixed at  $120^\circ\text{C}$ . Due to the low value of  $T_{\text{H}_2}$ , hydrogenolysis is negligible and cannot be made responsible for this mode of variation which, therefore, reflects a similar variation affecting the adlayer at the end of its formation. It is reasonable to assume that the proportion of the ethane precursor first diminishes versus  $T_{\text{CH}_4}$  because a larger fraction of it is involved in the formation of heavier adspecies. At  $T_{\text{CH}_4} > 240^\circ\text{C}$ , it is the reverse which holds and this cannot result but from a lesser tendency of the adspecies present on the surface to give rise to C–C bonding. The same kind of variation is observed in the case of the propane but the butanes and the pentanes display only a lowering in the range of  $T_{\text{CH}_4}$  we have explored. The proportion of the heptanes displays a variation which is just the opposite of that of the ethane since it increases first, goes through a maximum and decreases above

$240^\circ\text{C}$ . The initial increase is naturally due to the building up of the necessary amount of carbonaceous adspecies and is similar to that which would necessarily have been observed in the cases of the lighter adspecies if lower values of  $T_{\text{CH}_4}$  had been explored. The further decrease is ambiguous as it can be due to some lesser tendency of the lighter units to polymerize on and also to a partial conversion of  $\text{C}_7$  to  $\text{C}_8$  precursors since the proportion of the octanes in the products continues to increase, or to both factors. We can expect a variation of the octanes of the same type as that of the heptanes but shifted to higher temperatures which have not been explored in this work. We can also interpret the steeper decrease of the total  $\text{C}_{2+}$  production versus  $T_{\text{CH}_4}$  on Ru (Fig. 2), as compared to the corresponding one on Pt (Fig. 1), as being partially due to the assumed lessened tendency to polymerization exhibited by carbonaceous adspecies on the Ru surface if the temperature is increased.

So far, the present discussion as well as that developed in our preceding article (1) does not refer to the presence of species such as  $\text{C}_\alpha$ ,  $\text{C}_\beta$ , and  $\text{C}_\gamma$  on the catalyst, but, instead, to that of hydrocarbonaceous precursors of different weights. Figures 9a, 9b, and 10a show  $\text{H}_2$ -TPSR profiles, corresponding to Pt and Ru, respectively, and obtained after exposures of these metals similar to those used in this work. The hydrocarbons released at r.t. are not represented and we must remark that only the profiles of  $\text{CH}_4$ ,  $\text{C}_2\text{H}_6$ , and  $\text{C}_3\text{H}_8$  could be monitored since the duration of the complete chromatographic analysis was too long to allow us to monitor each product and to get the spectra of each of them. This is all the more regrettable as we know that all the hydrocarbons described in our work are evolved throughout the whole range of  $T_{\text{H}_2}$ . Complete analysis of the products contained in each sampling of the gas exiting the reactor during the heating of the catalyst requires time consuming work and needs special equipment. However, its interest prompts us to complete it in the near future. From the present profiles we can notice that, on Ru, the release of ethane paralleled that of methane (Fig. 10a). This was still more evident in the case of platinum, and even propane exhibited the same behavior (Figs. 9a and 9b). Clearly no unreactive carbon deposits *hydrogenated into methane only at temperatures higher than  $400^\circ\text{C}$*  were present, unless the exposure to  $\text{CH}_4$  was carried out under conditions of temperature and pressure favoring the  $\text{CH}_4$  decomposition (Fig. 10b).

Most of the results described in the present article and in our preceding one (1) can thus be reasonably interpreted if one assumes the existence of hydrocarbonaceous precursors of different weights and shapes at the end of the exposure to the methane, as we have done in our previous contributions (20–23). We cannot ascribe the origin of the  $\text{C}_{2+}$  products only to the deposit displaying the highest reactivity toward  $\text{H}_2$  and frequently reported as  $\text{C}_\alpha$ . It may even happen that the most reactive form of carbon, i.e. that able to be converted into  $\text{CH}_4$  at r.t., be present, without it

being possible to get  $C_{2+}$  products. This is the case when the catalyst is exposed to  $CH_4$  in a static way which does not allow a sufficient removal of  $H_2$  (21, 22). Deeper insight into the origin of the different species and the nature of their surface precursors could be supplied by detailed and complete  $H_2$ -TPSR spectra. Limited to the formation of  $CH_4$  only, the  $H_2$ -TPSR profiles constitute too crude a reactivity test. This is a conclusion akin to that already expressed by Biloen and Sachtler who considered that the role of carbidic carbon in methanation and Fischer–Tropsch reactions may have been overestimated (15).

The most reactive part of the carbonaceous deposits, i.e.  $C_\alpha$ , might consist of  $C_1$  adspecies, while the most unreactive part, i.e.  $C_\gamma$  when present, is probably graphitic carbon. However, if  $C_\alpha$  is assumed to consist of  $C_1$  adspecies (13) we must admit that the chain growth proceeds during the hydrogenation step, as in Fischer–Tropsch synthesis, whence a product distribution obeying the ASF (Anderson–Schultz–Flory) distribution. This was indeed the case in the results obtained by Koerts *et al.* (13). However, in the present work (including r.t. hydrogenations), large departures from the ASF distribution were always observed. This situation is not surprising if various precursors containing numerous C–C bonds build up during the exposure to  $CH_4$  and if, as can be reasonably expected, some of them are favored by the surface geometry (23). We must therefore admit either that  $C_\alpha$  is not made only of  $C_1$  adspecies or that a good part of the precursors containing several carbon atoms, and sometimes included in  $C_\beta$ , is as reactive as  $C_\alpha$ . What seems important is that, in our experimental conditions, numerous carbonaceous deposits displaying a broad range of reactivity build up during exposure of the catalyst to  $CH_4$ . The lighter precursors are able to react at r.t. while the heavier ones react at much higher temperatures.

A final remark is worth making. Most of the contributions devoted to this topic only report the formation of ethane, propane, and traces of higher products, which is in sharp contrast with our results. We think that the key condition for obtaining a good proportion of higher hydrocarbons is to allow the metal surface to reach substantial coverage with adequately dehydrogenated carbonaceous adspecies. Methyl adspecies are unable to give rise to C–C bonding and only lead to  $CH_4$  upon hydrogenation, as does graphitic carbon at much higher temperatures. Feeding the catalyst with  $CH_4$  for a long enough period of time at a moderate temperature, at not too low a pressure, and at a flow rate ensuring an adequate removal of  $H_2$  appears as favorite operating conditions. It is thanks to the use of such conditions that the preferential formation of  $C_{5+}$  hydrocarbons could

be obtained in our work as was the case in the contribution by Guzzi *et al.* (24).

## CONCLUSION

Systematic study of the products formed by hydrogenating, at a given temperature, the adlayers built up on Pt and Ru upon their exposure to  $CH_4$  at a higher temperature allows one to get significant insights into the likely composition of the adlayer and into its changes as a function of the temperature of adsorption of the methane. Several families of hydrocarbon precursors differing in their carbon content and in their shape are formed during the exposure to  $CH_4$ . Increasing the temperature of the exposure favors the formation of precursors of increasing weight on Pt, whereas, on Ru, this trend is counteracted by the opposite tendency to a lesser degree of polymerization.

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